AMENDMENTS TO THE CLAIMS

1. - 27. (cancelled).

28. (previously presented) A method for hydrorefining hydrocarbon feed oil including a sulfur-containing compound using at least two catalyst layers, comprising the steps of:

introducing hydrocarbon feed oil to the first catalyst layer together with hydrogen;

temporarily holding, by using a holding member, a liquid component that has flown out from the first catalyst layer, and stripping the liquid component with a first hydrogen gas stream that is fed from a hydrogen introduction part provided between the first catalyst layer and the second catalyst layer so that the first hydrogen gas stream passes through the liquid component as a countercurrent to the liquid component;

removing a vapor component that has been produced from the first catalyst layer and a vapor component that has been produced by stripping, while adjusting flow of the vapor component produced from the first catalyst layer and the vapor component produced by stripping in order to perform the stripping; and

introducing the stripped liquid component to the second catalyst layer together with and cocurrent with a second hydrogen gas stream that is fed from the hydrogen introduction part.

- 29. (previously presented) A hydrorefining method according to claim 28, wherein the holding member is a tray which has a liquid discharge hole and in which liquid component accumulates.
- 30. (previously presented) A hydrorefining method according to claim 28, wherein the holding member is a packing material through which the liquid component can pass.

Application No. 09/889,241 Amendment dated August 24, 2005 After Final Office Action of April 25, 2005

31. (previously presented) A hydrorefining method according to claim 28, wherein the

Docket No.: 2282-0142P

hydrocarbon feed oil is hydrocarbon oil in which 90 vol% distillation temperature is 250°C or

higher.

32. (previously presented) A hydrorefining method according to claim 28, wherein the

hydrocarbon feed oil has a 10 vol% distillation temperature of 220 to 300°C and a 90 vol%

distillation temperature of 320 to 380°C, and the hydrorefined hydrocarbon feed oil has a sulfur

content of not more than 150 ppm.

33. (cancelled).

34. (previously presented) The hydrorefining method of claim 28, comprising the further

step of recycling hydrogen recovered from the removed vapor component into a hydrogen gas

stream being introduced into the process.

35. (currently amended) A hydrorefining unit for hydrorefining hydrocarbon feed oil

including sulfur-containing compounds, comprising:

a first catalyst layer and a second catalyst layer;

a holding member positioned between the first catalyst layer and second catalyst layer for

temporarily holding a liquid component that flows out from the first catalyst layer, wherein said

holding member is a valve tray;

a hydrogen feed source;

a hydrogen introduction part, that is connected to the hydrogen feed source, for

simultaneously introducing hydrogen from the hydrogen feed source to the liquid component

held in the holding member and the second catalyst layer, wherein the hydrogen introduced from

the hydrogen introduction part has a first hydrogen gas stream and a second hydrogen gas

stream;

a separation space that is positioned at the bottom of the first catalyst layer for separation

of vapor component and

Birch, Stewart, Kolasch & Birch, LLP

3

Application No. 09/889,241 Amendment dated August 24, 2005 After Final Office Action of April 25, 2005

liquid component;

means for adjusting pressure of the separation space and/or a space between the holding

member and the second catalyst layer; and

a gas outlet through which the vapor component is discharged from the separation space.

Docket No.: 2282-0142P

36. (previously presented) A hydrorefining unit according to claim 35, wherein said

means for adjusting pressure comprises a flow meter and flow adjustment valve that are

operatively connected to said gas outlet.

37. (previously presented) A hydrorefining unit according to claim 35, further comprising

means for recycling hydrogen from the discharged vapor component into the hydrogen

introduction part.

38. (previously presented) A hydrorefining unit according to claim 35, wherein the first

catalyst layer, second catalyst layer, and holding member are housed in a single reaction vessel.

39. (previously presented) A hydrorefining unit according to claim 35, wherein the

holding member is a tray which has a discharge hole for liquid component and in which liquid

component accumulates.

40. (cancelled).

41. (previously presented) A hydrorefining unit according to claim 35, wherein impurities

are stripped from the liquid component held in the holding member by the first hydrogen gas

stream.

42. (previously presented) A hydrorefining unit according to claim 41, wherein the

impurities are hydrogen sulfide and/or ammonia.

Birch, Stewart, Kolasch & Birch, LLP

4

Application No. 09/889,241
Amendment dated August 24, 2005

After Final Office Action of April 25, 2005

43. (currently amended) A hydrorefining unit for hydrorefining hydrocarbon feed oil including sulfur-containing compounds, comprising:

Docket No.: 2282-0142P

a first catalyst layer and a second catalyst layer;

a holding member positioned between the first catalyst layer and second catalyst layer for temporarily holding a liquid component that flows out from the first catalyst layer, wherein said holding member is a valve tray;

a hydrogen feed source;

a hydrogen introduction part, that is connected to the hydrogen feed source, for simultaneously introducing hydrogen from the hydrogen feed source to the liquid component held in the holding member and the second catalyst layer;

a separation space that is positioned at the bottom of the first catalyst layer for separation of vapor component and

liquid component, wherein the separation space and/or a space between the holding member and the second catalyst layer can have its pressure adjusted; and

a gas outlet through which the vapor component is discharged from the separation space.

44. (previously presented) A hydrorefining unit according to claim 43, comprising a flow meter and flow adjustment valve operatively connected to said gas outlet for the adjustment of pressure in the separation space and/or the space between the holding member and the second catalyst layer.

45. (previously presented) A hydrorefining unit according to claim 43, further comprising means for recycling hydrogen from the discharged vapor component into the hydrogen introduction part.

46. (previously presented) A hydrorefining method according to claim 28, wherein the holding member is a valve tray.

47. (cancelled).

Birch, Stewart, Kolasch & Birch, LLP

5

Application No. 09/889,241 Amendment dated August 24, 2005 After Final Office Action of April 25, 2005

48. (cancelled).

Docket No.: 2282-0142P